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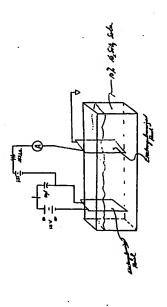
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(54) TILE: AN ELECTROLYTIC PROCESS FOR FORMING A MINERAL CONTAINING COATING

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(57) Abstract

The disclosure relates to a process for forming a deposit on the surface of a metallic or conductive surface. The process employs an electrolytic process to deposit a mineral containing conting or film upon a metallic or conductive surface.

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AN ELECTROLYTIC PROCESS FOR FORMING A MINERAL CONTAINING COATING

35 U.S.C. 119(e) and 35 U.S.C. 120 of U.S. Provisional Patent Application Serial May 2, 1997 and entitled "Non-Equilibrium Enhanced Mineral Deposition". The The subject matter of this invention claims benefit under 35 U.S.C. 111(a), Nos. 60/036,024, filed on January 31, 1997 and Serial No. 60/045,446, filed on disclosure of the previously filed provisional patent applications is hereby incorporated by reference.

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FIELD OF THE INVENTION

surface of a metallic or conductive surface. The process employs an electrolytic The instant invention relates to a process for forming a deposit on the process to deposit a mineral containing coating or film upon a metallic or conductive surface. 2

BACKGROUND OF THE INVENTION

prior to an electroplating operation. Using "Silicates As Cleaners In The Production of Tinplate" is described by L.J. Brown in February 1966 edition of among other surfaces. Electrocleaning is typically employed as a cleaning step Silicates have been used in electrocleaning operations to clean steel, tin, ន

Processes for electrolytically forming a protective layer or film by using an anodic method are disclosed by U.S. Patent No. 3,658,662 (Casson, Jr. et al.), and United Kingdom Patent No. 498,485; both of which are hereby incorporated by reference

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U.S. Patent No. 5,352,342 to Riffe, which issued on October 4, 1994 and is entitled "Method And Apparatus For Preventing Corrosion Of Metal Structures" that describes using electromotive forces upon a zinc solvent containing paint. 8

SUMMARY OF THE INVENTION

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electrically conductive substrate into a silicate containing bath wherein a current is crystals forms upon the substrate. The mineral layer imparts improved corrosion metallic substrate. The cathodic method is normally conducted by immersing a practices by providing a cathodic method for forming a protective layer upon a comprising an amorphous matrix surrounding or incorporating metal silicate The instant invention solves problems associated with conventional pased through the bath and the substrate is the cathode. A mineral layer resistance, among other properties, to the underlying substrate.

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methods by obviating the need for solvents or solvent containing systems to form a corrosion resistant layer, i.c., a mineral layer. In contrast, to conventional methods the inventive process is substantially solvent free. By "substantially solvent free" volatile organic compounds (V.O.C.s) are present in the electrolytic environment. The inventive process is also a marked improvement over conventional it is meant that less than about 5 wt.%, and normally less than about 1 wt.%

In contrast to conventional electrocleaning processes, the instant invention oxide containing products such as greenalite whereas the instant invention relates substrate. Conventional electrocleaning processes sought to avoid formation of employs silicates in a cathodic process for forming a mineral layer upon the to a method for forming silicate containing products, i.e., a mineral. 2

CROSS REFERENCE TO RELATED PATENTS

AND PATENT APPLICATIONS

08/634,215 (filed on April 18, 1996) in the names of Robert L. Heimann et al., and 08/791,337 (Attorney Docket No. EL001RH-4 filed on January 31, 1997) in the The subject matter of the instant invention is related to copending and EL001RH-8), filed respectively on May 2, 1997 and even date herewith, and entitled "Corrosion Resistant Buffer System for Metal Products", which is a continuation in part of Non-Provisional U.S Patent Application Serial No. names of Robert L. Heimann et al., as a continuation in part of Serial No. commonly assigned Non-Provisional U.S. Patent Application Serial Nos. (EL001RH-6, EL001RH-7 and 08/476,271 (filed on June 7, 1995) in the names of Heimann et al., and 08/850,323; 08/850,586; and 2 2

corresponding to WIPO Patent Application Publication No. WO 96/12770, which in turn is a continuation in part of Non-Provisional U.S. Patent Application Serial No. 08/327,438 (filed on October 21, 1994), now allowed. 23

date herewith and entitled "Corrosion Protective Coatings". The subject matter of (Attorney Docket No. EL004RH-1), filed on even The subject matter of this invention is related to Non-Provisional Patent this invention is also related to Non-Provisional Patent Application Serial No. Application Serial No. 8

herewith and January 31, 1997 and entitled "Aqueous Gel Compositions and Use Thereof". The disclosure of the previously identified patents, patent applications (Attorney Docket No. EL005NM-1), filed respectively, on even date and publications is hereby incorporated by reference.

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BRIEF DESCRIPTION OF THE DRAWING

Figure 1 is a schematic drawing of the circuit and apparatus which can be employed for practicing an aspect of the invention.

DETAILED DESCRIPTION

soluble mineral components, and utilizes an electrically enhanced method to obtain Copending and Commonly Assigned Patents and Patent Applications; incorporated formed upon a metal or conductive surface wherein at least a portion of the coating containing coating," it is meant to refer to a relatively thin coating or film which is or film includes at least one of metal atom containing mineral, e.g., an amorphous phase or matrix surrounding or incorporating crystals comprising a zinc disilicate. by reference. By "electroyltic" or "electrodeposition" or "electrically enhanced", mineral containing coating or film upon a metallic or an electrically conductive a mineral coating or film upon a metallic or conductive surface. By "mineral surface. The process employs a mineral containing solution e.g., containing it is meant to refer to an environment created by passing an electrical current The instant invention relates to a process for depositing or forming a through a silicate containing medium while in contact with an electrically Mineral and Mineral Containing are defined in the previously identified conductive substrate wherein the substrate functions as the cathode.

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including immersing the substrate, applying a silicate containing coating upon the preferred method for establishing the environment will be determined by the size The electroyltic environment can be established in any suitable manner of the substrate, electroplating time, among other parameters known in the substrate and thereafter applying an electrical current, among others. The electrodeposition art.

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The silicate containing medium can be a fluid bath, gel, spray, among other methods for contacting the substrate with the silicate medium. Examples of the comprising at least one alkali silicate and a thickener, among others. Normally, silicate medium comprise a bath containing at least one alkali silicate, a gel the medium comprises a bath of sodium silicate.

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the inventive process can be employed to coat a wide range of metal surfaces, e.g., the group consisting of galvanized surfaces, zinc, iron, steel, brass, copper, nickel, Examples of suitable metal surfaces comprise at least one member selected from copper, aluminum and ferrous metals, the mineral layer can be formed on a non-The metal surface refers to a metal article as well as a non-metallic or an tin, aluminum, lead, cadmium, magnesium, alloys thereof, among others. While Conductive surfaces can also include carbon or graphite as well as conductive electrically conductive member having an adhered metal or conductive layer. conductive substrate having at least one surface coated with an electrically conductive material, e.g., a ceramic material encapsulated within a metal. polymers (polyaniline for example).

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The mineral coating can enhance the surface characteristics of the metal or example) from oxidation and improve bonding strength in composite materials, conductive surface such as resistance to corrosion, protect carbon (fibers for

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and reduce the conductivity of conductive polymer surfaces including potential application in sandwich type materials.

surface, is coated electrolytically by being placed into an aqueous sodium silicate solution. After being placed into the silicate solution, a mineral coating or film In an aspect of the invention, an electrogalvanized panel, e.g., a zinc

formed on the surface. Examples of suitable pretreatments comprise at least one of In one aspect of the invention, the metal surface, e.g., zinc, steel or lead, has facilitate acceptance of the mineral or silicate containing coating e.g., the inventive resistant coil steel. The particular pretreatment will be a function of composition of process can be employed as a step in a continuous process for producing corrosion the metal surface and desired composition of mineral containing coating/film to be process for conditioning the metal surface to clean it and condition the surface to been pretreated. By "pretreated" it is meant to refer to a batch or continuous cleaning, activating, and rinsing. A suitable pretreatment process for steel containing silicates is deposited by using low voltage and low current. 2 S 2

1) 2 minute immersion in a 3:1 dilution of Metal Prep 79 (Parker Amchem),

 10 second immersion in a pH 14 sodium hydroxide solution, 2) two deionized rinses,

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comprises:

4) remove excess solution and allow to air dry,

5) 5 minute immersion in a 50% hydrogen peroxide solution,

remove excess solution and allow to air dry.

anodically cleaning the surface. Such cleaning can be accomplished by immersing phosphates and carbonates. By using the work piece as the anode in a DC cell and maintaining a current of 100mA/cm2, this process can generate oxygen gas. The oxygen gas agitates the surface of the workpiece while oxidizing the substrate's the work piece or substrate into a medium comprising silicates, hydroxides, in another aspect of the invention, the metal surface is pretreated by ะ 8

zircon, vanadium, phosphorus, aluminum, iron, boron, bismuth, gallium, tellurium, aluminum and iron can be employed along with or instead of a silicate. The dopant include one or more dopant materials. While the cost and handling characteristics of sodium silicate are desirable, at least one member selected from the group of materials can be introduced to the metal or conductive surface in pretreatment germanium, antimony, niobium (also known as columbium), magnesium and In a further aspect of the invention, the silicate solution is modified to water soluble salts and oxides of tungsten, molybdenum, chromium, titanium manganese, mixtures thereof, among others, and usually, salts and oxides of steps prior to electrodeposition, in post treatment steps following

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electrodeposition, and/or by alternating electrolytic dips in solutions of dopants **4**

metal or conductive surface, e.g. an aqueous sodium silicate solution containing solution can be employed to form tailored mineral containing surfaces upon the water soluble dopants. When sodium silicate is employed as a mineral solution, Philadelphia Quartz (PQ) Corporation. The presence of dopants in the mineral and solutions of silicates if the silicates will not form a stable solution with the desirable results can be achieved by using N grade sodium silicate supplied by aluminate can be employed to form a layer comprising oxides of silicon and aluminum

polymers, and the eletrodeposition solution itself can be in the form of a flowable composition comprising 3 wt% N-grade Sodium Silicate Solution (PQ Corp), 0.5 thereof, among others. Further, the aqueous silicate solution can be filled with a polymer composite coating. The characteristics of the electrodeposition solution can be modified or tailored by using an anode material as a source of ions which wt% Carbopol EZ-2 (BF Goodrich), about 5 to 10 wt.% fumed silica, mixtures can be available for codeposition with the mineral anions and/or one or more water dispersible polymer such as polyurethane to electro deposit a mineraldopants. The dopants can be useful for building additional thickness of the The silicate solution can also be modified by adding water soluble gel consistency. A suitable composition can be obtained in an aqueous electrodeposited mineral layer.

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tailoring the inventive process to obtain a desirable mineral containing coating: The following sets forth the parameters which may be employed for

1.Voltage

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- Current Density
- 3. Apparatus or Cell Design 4. Deposition Time ห
- 5. Concentration of the N-grade sodium silicate solution
 - 7. Type and concentration of anions in solution
- 8. Type and concentration of cations in solution
 - - 9. Composition of the anode ន្ត
- 10. Composition of the cathode
 - 11. Temperature 12. Pressure
- 13. Type and Concentration of Surface Active Agents

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deposited on and the intended composition to be deposited. Items 1, 2, 7, and 8 can coating. That is, items 1 and 2 can affect the deposition time and coating thickness desirable chemical characteristics to the coating. The differing types of anions and be especially effective in tailoring the chemical and physical characteristics of the The specific ranges of the parameters above depend on the substrate to be whereas items 7 and 8 can be employed for introducing dopants that impart

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Group I metals, Group II metals, transition and rare earth metal oxides, oxyanions cations can comprise at least one member selected from the group consisting of such as mineral, molybdate, phosphate, titanate, boron nitride, silicon carbide, aluminum nitride, silicon nitride, mixtures thereof, among others.

replacing conventional phosphating process, e.g., in the case of automotive metal combined with or replace conventional metal finishing practices. The inventive mineral layer can be employed to protect a metal finish from corrosion thereby While the above description places particular emphasis upon forming a mineral containing layer upon a metal surface, the inventive process can be polyurethane based solution containing soluble silicates and employed as a aforementioned aqueous mineral solution can be replaced with an aqueous finishing the inventive process could be utilized instead of phosphates and chromates and prior to coating application e.g., E-Coat. Further, the 2

process. Moreover, depending upon the dopants and concentration thereof present microelectronic films, e.g., on metal or conductive surfaces in order to impart enhanced electrical and corrosion resistance, or to resist ultraviolet light and replacement for the so-called automotive E-coating and/or powder painting in the mineral deposition solution, the inventive process can produce monotomic oxygen containing environments such as space. 2

employed to fabricate corrosion resistant metal products that conventionally utilize zinc as a protective coating, e.g., automotive bodies and components, grain silos, end-uses such as in conventional plating operations as well as being adaptable to The inventive process can be employed in a virtually unlimited array of field service. For example, the inventive mineral containing coating can be

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Examples demonstrate the presence of a unique metal disilicate species within the mineralized layer, e.g., ESCA measures the binding energy of the photoelectrons The x-ray photoelectron spectroscopy (ESCA) data in the following bridges, among many other end-uses. n

invention and it is understood that such an Example does not limit the scope of the The following Examples are provided to illustrate certain aspects of the of the atoms present to determine bonding characteristics. invention as defined in the appended claims. 8

The following apparatus and materials were employed in this Example:

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Standard Electrogalvanized Test Panels, ACT Laboratories 10% (by weight) N-grade Sodium Mineral solution 12 Volt EverReady battery

1.5 Volt Ray-O-Vac Heavy Duty Dry Cell Battery Friplett RMS Digital Multimeter 6

30 µF Capacitor 29.8 kΩ Resistor

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aforementioned test panels were contacted with a solution comprising 10% sodium practicing the Example are illustrated in Figure 1. Referring now to Figure 1, the solution in the manner illustrated in Figure 1. The test panels was exposed for 74 hours under ambient environmental conditions. A visual inspection of the panels indicated that a light-grey colored coating or film was deposited upon the test mineral and deionized water. A current was passed through the circuit and A schematic of the circuit and apparatus which were employed for

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the coated area was exposed and, thereafter, the taped panels were placed into salt Mineral Solution. In addition, bare zinc phosphate coated steel panels (ACT B952, Procedure No. B117. A section of the panels was covered with tape so that only no Parcolene) and bare iron phosphate coated steel panels (B1000, no Parcolene) accordance with ASTM Procedure No. B117, 1) Bare Electrogalvanized Panel, spray. For purposes of comparison, the following panels were also tested in containing coating, the coated panels were tested in accordance with ASTM In order to ascertain the corrosion protection afforded by the mineral and 2) Bare Electrogalvanized Panel soaked for 70 hours in a 10% Sodium were subjected to salt spray for reference.

The results of the ASTM Procedure are listed in the Table below:

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240+	Coated Cathode of the Invention
	Soak
≈ 120	Standard Panel with Sodium Mineral
≈ 120	Standard Bare Electrogalvanize Panel
1	Iron phosphate coated steel
1	Zinc phosphate coated steel
Hours in B117 Salt Spray	Panel Description

The above Table illustrates that the instant invention forms a coating or film which imparts markedly improved corrosion resistance. It is also apparent that the process has resulted in a corrosion protective film that lengthens the life of electrogalvanized metal substrates and surfaces. ង

ESCA analysis was performed on the zinc surface in accordance with conventional techniques and under the following conditions:

Analytical conditions for ESCA:

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Instrument

Physical Electronics Model 5701 LSci

C-(C,H) in C 1s spectra at 284.6 eV Monochromatic aluminum electron flood gun 2 mm X 0.8 mm 350 watts 20° ±1% Electron acceptance angle Charge neutralization Charge correction Analysis region Source power X-ray source Exit angle*

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* Exit angle is defined as the angle between the sample plane and the electron

analyzer lens. 2

This species was identified as a zinc disilicate modified by the presence of sodium The silicon photoelectron binding energy was used to characterized the nature of the formed species within the mineralized layer that was formed on the cathode.

ion by the binding energy of 102.1 eV for the Si(2p) photoelectron.

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EXAMPLE 2

This Example illustrates performing the inventive electrodeposition process at an increased voltage and current in comparison to Example 1.

Prior to the electrodeposition, the cathode panel was subjected preconditioning process: 2

1) 2 minute immersion in a 3:1 dilution of Metal Prep 79 (Parker Amchem)

2) two deionized rinse,

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3) 10 second immersion in a pH 14 sodium hydroxide solution,

remove excess solution and allow to air dry,

5) 5 minute immersion in a 50% hydrogen peroxide solution,

6) Blot to remove excess solution and allow to air dry.

panels. One end of the test panel was immersed in a solution consisting of 10% N grade sodium mineral (PQ Corp.) in deionized water. The immersed area (1 side) to cathode ratio. The panels were connected directly to the DC power supply and a A power supply was connected to an electrodeposition cell consisting of a of each panel was approximately 3 inches by 4 inches (12 sq. in.) for a 1:1 anode voltage of 6 volts was applied for 1 hour. The resulting current ranged from approximately 0.7-1.9 Amperes. The resultant current density ranged from 0.05plastic cup containing two standard ACT cold roll steel (clean, unpolished) test 0.16 amps/in 35 8

After the electrolytic process, the coated panel was allowed to dry at ambient conditions and then evaluated for humidity resistance in accordance with ASTM Test No. D2247 by visually monitoring the corrosion activity until **\$**

development of red corrosion upon 5% of the panel surface area. The coated test panels lasted 25 hours until the first appearance of red corrosion and 120 hours until 5% red corrosion. In comparison, conventional iron and zinc phosphated steel panels develop first corrosion and 5% red corrosion after 7 hours in ASTM D2247 humidity exposure. The above Examples, therefore, illustrate that the inventive process offers an improvement in corrosion resistance over iron and zinc phosphated steel panels.

EXAMPLE 3

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placed in a solution comprising 1 wt.% N-grade sodium silicate (supplied by PQ cleaned in 6M HCl for 25 minutes. The cleaned lead panels were subsequently Two lead panels were prepared from commercial lead sheathing and Corporation).

panels were removed from the sodium silicate solution and rinsed with deionized One lead panel was connected to a DC power supply as the anode and the other was a cathode. A potentional of 20 volts was applied initially to produce a current ranging from 0.9 to 1.3 Amperes. After approximately 75 minutes the

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disilicate modified by the presence of sodium ion by the binding energy of 102.0 photoelectron binding energy was used to characterized the nature of the formed species within the mineralized layer. This species was identified as a lead ESCA analysis was performed on the lead surface. The silicon eV for the Si(2p) photoelectron. 2

EXAMPLE 4

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were reacted to form the metal silicate surface. Two different alloys of aluminum electrolytic process, each panel was prepared using the methods outlined below in panel as an anode into an aqueous solution containing 5% NaOH, 2.4% Na₂CO₃, This Example demonstrates forming a mineral surface upon an aluminum Table A. Each panel was washed with reagent alcohol to remove any excessive anodic cleaning or both. Both forms of cleaning are designed to remove excess substrate. Using the same apparatus in Example 1, aluminum coupons (3" x 6") dirt and oils. The panels were either cleaned with Alumiprep 33, subjected to aluminum oxides. Anodic cleaning was accomplished by placing the working density of 100mA/cm² across the immersed area of the panel for one minute. 2% Na₂SiO₃, 0.6% Na₃PO₄, and applying a potential to maintain a current were used, Al 2024 and Al7075. Prior to the panels being subjected to the

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power supply by a wire while another panel was attached to the positive lead. The are shown in the table below. The panel was attached to the negative lead of a DC Once the panel was cleaned, it was placed in a lliter beaker filled with 800 mL of solution. The baths were prepared using deionized water and the contents

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two panels were spaced 2 inches apart from each other. The potential was set to

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the voltage shown on the table and the cell was run for one hour.

			TABI	LEA				
Example	Y.	В	၁	C D		F	G	
Alloy type	2024	2024	2024	2024	7075	7075	7075	7075
Anodic	Yes	Yes	ŝ	å		Yes	ŝ	
Cleaning								
Acid Wash	Yes							
Bath Solution								
Na ₂ SiO ₃	%	%01	%	10%	%	10%	%	10%
H ₂ O ₂	%!	%	%	%!	%	%	%	%
Potential	12V	18V	12V	18V	12V	180	12V	187

silicates of the coating. It is also believed that the silica is a result of either excess The metal silicate is indicated by a Si (2p) binding energy (BE) in the low 102 eV silicates from the reaction or precipitated silica from the coating removal process. sample measured showed a mixture of silica and metal silicate. Without wishing to be bound by any theory or explanation, it is believed that the metal silicate is a range, typically between 102.1 to 102.3. The silica can be seen by Si(2p) BE ESCA was used to analyze the surface of each of the substrates. Every result of the reaction between the metal cations of the surface and the alkali

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deconvolution reveal binding energies in the ranges representative of metal silicate between 103.3 to 103.6 eV. The resulting spectra show overlapping peaks, upon and silica.

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EXAMPLE 5

This Example illustrates an alternative to immersion for creating the silicate An aqueous gel made from 5% sodium silicate and 10% fumed silica was containing medium.

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by a sodium hydroxide wash and a hydrogen peroxide bath. The apparatus was set up using a DC power supply connecting the positive lead to the steel panel and the while the other panel was washed in a phosphoric acid based metal prep, followed designed to simulate a brush plating operation. The "brush" was immersed in the used to coat cold rolled steel panels. One panel was washed with reagent alcohol gel solution to allow for complete saturation. The potential was set for 12V and the gel was painted onto the panel with the brush. As the brush passed over the negative lead to a platinum wire wrapped with glass wool. This setup was 23 2

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surface of the panel, hydrogen gas evolution could be seen. The gel was brushed on for five minutes and the panel was then washed with DI water to remove any excess gel and unreacted silicates.

ESCA was used to analyze the surface of each steel panel. ESCA detects the reaction products between the metal substrate and the environment created by the electrolytic process. Every sample measured showed a mixture of silica and metal silicate. The metal silicate is a result of the reaction between the metal cations of the surface and the alkali silicates of the coating. The silica is a result of either excess silicates from the reaction or precipitated silica from the coating emenval process. The metal silicate is indicated by a Si (2p) binding energy (BE) in the low 102 eV range, typically between 102.1 to 102.3. The silica can be seen by Si(2p) BE between 103.3 to 103.6 eV. The resulting spectra show overlapping peaks, upon deconvolution reveal binding energies in the ranges representative of metal silicate and silica.

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EXAMPLE 6

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Using the same apparatus in Example 1, cold rolled steel coupons (ACT laboratories) were reacted to form the metal silicate surface. Prior to the panels being subjected to the electrolytic process, each panel was prepared using the methods outlined below in Table B. Each panel was washed with reagent alcohol to remove any excessive dirt and oils. The panels were either cleaned with Metalprep 79 (Parker Amchem), subjected to anodic cleaning or both. Both forms of cleaning are designed to remove excess metal oxides. Anodic cleaning was accomplished by placing the working panel as an anode into an aqueous solution containing 5% NaOH, 2.4% Na₂CO₃, 2% Na₂SiO₃, 0.6% Na₃PO₄, and applying a potential to maintain a current density of 100mA/cm² across the immersed area of the panel for one minute.

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Once the panel was cleaned, it was placed in a liter beaker filled with 800 mL of solution. The baths were prepared using deionized water and the contents are shown in the table below. The panel was attached to the negative lead of a DC power supply by a wire while another panel was attached to the positive lead. The two panels were spaced 2 inches apart from each other. The potential was set to the voltage shown on the table and the cell was run for one hour.

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RSZ 22 _{ဆို} ဆို SS S % ဗ ŝ TABLE B 10% CRS Ϋ́ SRS No Ϋ́ς % ≨ Anodic Cleaning Substrate type **Bath Solution** Acid Wash Na₂SiO₃ Example

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•	•	0.25 hr
•	•	0.25 hr
(CV)	8248	된
6 (CV)	23-10	본
14-24	23 (CC)	2hrs
Potential (V)	Current Density (mA/cm ²)	B177

1 Cold Rolled Steel Control- No treatment was done to this panel.

2 Cold Rolled Steel with iron phosphate treatment (ACT Laboratories)- No further treatments were performed

The electrolytic process was either run as a constant current or constant voltage experiment, designated by the CV or CC symbol in the table. Constant Voltage experiments applied a constant potential to the cell allowing the current to fluctuate while Constant Current experiments held the current by adjusting the potential. Panels were tested for corrosion protection using ASTM B117. Failures were determined at 5% surface coverage of red rust.

2

ESCA was used to analyze the surface of each of the substrates. ESCA detects the reaction products between the metal substrate and the environment created by the electrolytic process. Every sample measured showed a mixture of silica and metal silicate. The metal silicate is a result of the reaction between the metal eations of the surface and the alkali silicates of the coating. The silica is a result of either excess silicates from the reaction or precipitated silica from the coating removal process. The metal silicate is indicated by a Si (2p) binding energy (BE) in the low 102 eV range, typically between 102.1 to 102.3. The silica can be seen by Si(2p) BE between 103.3 to 103.6 eV. The resulting spectra show overlapping preaks, upon deconvolution reveal binding energies in the ranges representative of metal silicate and silica.

EXAMPLE 7

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Using the same apparatus in Example 1, zinc galvanized steel coupons (EZG 60G ACT Laboratories) were reacted to form the metal silicate surface. Prior to the panels being subjected to the electrolytic process, each panel was prepared using the methods outlined below in Table C. Each panel was with reagent alcohol to remove any excessive dirt and oils.

Once the panel was cleaned, it was placed in a 1 liter beaker filled with 800 mL of solution. The baths were prepared using deionized water and the contents are shown in the table below. The panel was attached to the negative lead of a DC power supply by a wire while another panel was attached to the positive lead. The two panels were spaced approximately 2 inches apart from each other. The

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potential was set to the voltage shown on the table and the cell was run for one

hour.

		TABLEC	ပ		
Example	Αl	B2	ខ	DS	
Substrate type Bath Solution	SĐ	CS	SS	GSI	
Na ₂ SiO ₃	%01	%	10%		
Potential (V)	(ري و	10 (CV)	18 (CV)		
Current Density	22-3	7-3	142-3		
(mA/cm^2)				٠	
B177	336 hrs	224 hrs	216 hrs	96 hrs	

1 IGalvanized Steel Control- No treatment was done to this panel.

Panels were tested for corrosion protection using ASTM B117. Failures were determined at 5% surface coverage of red rust.

2

energy (BE) in the low 102 eV range, typically between 102.1 to 102.3. The silica can be seen by Si(2p) BE between 103.3 to 103.6 eV. The resulting spectra show overlapping peaks, upon deconvolution reveal binding energies in the ranges created by the electrolytic process. Every sample measured showed a mixture of silica and metal silicate. The metal silicate is a result of the reaction between the metal cations of the surface and the alkali silicates of the coating. The silica is a result of either excess silicates from the reaction or precipitated silica from the ESCA was used to analyze the surface of each of the substrates. ESCA detects the reaction products between the metal substrate and the environment coating removal process. The metal silicate is indicated by a Si (2p) binding representative of metal silicate and silica. 2

2

EXAMPLE 8

panels being subjected to the electrolytic process, each panel was prepared using the methods outlined below in Table D. Each panel was washed with reagent Fullerton Metals) were reacted to form the metal silicate surface. Prior to the Using the same apparatus in Example 1, copper coupons (C110 Hard, alcohol to remove any excessive dirt and oils.

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are shown in the table below. The panel was attached to the negative lead of a DC power supply by a wire while another panel was attached to the positive lead. The Once the panel was cleaned, it was placed in a lliter beaker filled with 800 mL of solution. The baths were prepared using deionized water and the contents

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two panels were spaced 2 inches apart from each other. The potential was set to the voltage shown on the table and the ceil was run for one hour.

		TABLED	Ω		
Example	Ψ	BB2	CC3	DD4	EES
Substrate type	n O	ਠੌ	ວັ	ر ت	CuI
Bath Solution					
Na ₂ SiO ₃	10%	10%	%	1%	•
Potential (V)	12 (CV)	6(CV)	6 (CV)	36 (CV)	•
Current Density	40-17	19-9	1	36-10	•
(mA/cm ²)					
B117	11 hrs	11 hrs	5 hrs	5 hrs	2 hrs

! Copper Control- No treatment was done to this panel.

Panels were tested for corrosion protection using ASTM B117. Failures were determined by the presence of copper.oxide which was indicated by the

between the metal cations of the surface and the alkali silicates of the coating. The environment set up from the electrolytic process. Every sample measured showed a mixture of silica and metal silicate. The metal silicate is a result of the reaction binding energy (BE) in the low 102 eV range, typically between 102.1 to 102.3. silica is a result of either excess silicates from the reaction or precipitated silica allows us to examine the reaction products between the metal substrate and the The silica can be seen by Si(2p) BE between 103.3 to 103.6 eV. The resulting ESCA was used to analyze the surface of each of the substrates. ESCA from the coating removal process. The metal silicate is indicated by a Si (2p) appearance of a dull haze over the surface. 2 2

spectra show overlapping peaks, upon deconvolution reveal binding energies in the ranges representative of metal silicate and silica. ឧ

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THE FOLLOWING IS CLAIMED.

1. An electrically enhanced method for forming a corrosion resistant surface on a metal surface comprising:

passing a current through said surface and medium at a rate and period of time sufficient to form a mineral upon the surface wherein said mineral imparts improved corrosion resistance to said surface. contacting the metal surface with a silicate containing medium,

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2. A method for improving the corrosion resistance of an electrically conductive surface comprising:

2

passing a current through said surface and medium wherein said metal surface reacts with a portion of the metal surface to form a layer having improved immersing the metal surface within an alkali silicate containing medium, corrosion resistance in comparison to the metal surface.

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3. A cathodic method for improving the corrosion resistance of metal surface comprising:

establishing an electroylitic environment wherein the surface is employed exposing the metal surface to a silicate containing medium,

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passing a current through the silicate medium and the surface for a period of time and under conditions sufficient to form a corrosion resistant surface upon the metal surface. as a cathode,

4. The method of Claim 3 wherein the silicate containing medium comprises sodium silicate.

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5. The method of Claim 3 wherein the metal surface comprises at least one member selected from the group consisting of lead, copper, zinc, aluminum and ខ្ល

comprises a reaction product formed between the metal surface and the silicate. 6. The method of Claim 3 wherein the corrosion resistant surface

7. The method of Claim 6 wherein the corrosion resistant surface comprises a mineral layer.

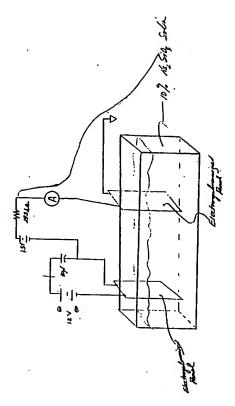
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INTERNATIONAL, SEARCH REPORT

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A. CLASS. IPC 6	A. CLASSIFICATION OF BUBLECT MATTER IPC 6 C2509/04			
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According to	According to Intermational Patent Classification (IPC) or to both national classification and IPC			
8. FIELDS	B. FIELDS SEARCHED			
IPC 6	Mohaman documentation sewarched (desemblation system lottowed by classification symbols) $1PC \in C25D$			
Documents	Documentation eserched other than makimum documentation to the scient that each documents are included in the fields executed	betthe searched		
Electronio d	Electronic data base consulted during the triannational search (name of data base and, where practical, search lerms used)	(Deen su		
C. DOCUM	C. DOCUMENTS CONSIDERED TO BE RELEVANT			
Cathgory *	Childon of document, with indication, where appropriate, of the relevant passages	A. A.	Relevant to claim No.	
×	US 3 658 662 A (CASSON EDWARD A JR ET AL) 25 April 1972 cited in the application see column 1, line 1-3; claims 1-5	1,2		
× '	DATABASE WPI Section Ch. Neek 9344 Class M11, AN 93-348855 XPODZOGS862 & JP 05 255 889 A (KANASAKI STEEL CORP) see abstract		_	
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INTERNATIONAL SEARCH REPORT

ition No	Publication	15-11-1972 28-05-1970 15-05-1973 29-02-1972 30-07-1970	04-10-1972 23-07-1970 25-08-1971
Inter and Application No PCT/US 98/01682		304216 A 743794 A 926335 A 519586 A 2000227 A	444
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IN I EKNA I JONAL SEARCH	Publication date	25-04-1972	
thought.	Patent document cited in search report	US 3658662 A	

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Van Leeuwen, R

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26 May 1998

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Further documents are tated in the continuation of box C.